- The Lumped Capacitance Method  $5.1$
- $5.2$ Validity of the Lumped Capacitance Method
- General Lumped Capacitance Analysis  $5.3$ 
	- 5.3.1 Radiation Only 288
	- 5.3.2 Negligible Radiation 288
	- 5.3.3 Convection Only with Variable Convection Coefficient



#### *3. General Lumped Capacitance Analysis*

- $\triangleright$  The figure below shows the general situation for which thermal conditions within a solid may be influenced simultaneously by convection, radiation, an applied surface heat flux, and internal energy generation.
- *To study this system, the general Lumped Capacitance Analysis is needed.*



$$
q_s''A_{s,h} + \dot{E}_g - (q_{\text{conv}}'' + q_{\text{rad}}'')A_{s(c,r)} = \rho Vc \frac{dT}{dt}
$$

$$
q_s''A_{s,h} + \dot{E}_g - [h(T - T_\infty) + \varepsilon \sigma (T^4 - T_{sur}^4)]A_{s(c,r)} = \rho Vc \frac{dT}{dt}
$$

The transient conduction in a solid studied before, was initiated by convection heat transfer to or from an adjoining fluid.

#### *3. General Lumped Capacitance Analysis A. Only Radiation:*



#### *3. General Lumped Capacitance Analysis B. No Radiation:*

$$
q_s''A_{s,h} + \dot{E}_g - [h(T - T_\infty) + \mathbf{e}\sigma(T^4 - T_{sur}^4)]A_{s(c)} = \rho Vc \frac{dT}{dt}
$$

$$
\frac{d\theta}{dt} + a\theta - b = 0 \qquad a \equiv (hA_{s,c}/\rho Vc) \qquad b \equiv [(q''_sA_{s,h} + \dot{E}_g)/\rho Vc]
$$

This equation is a linear, first-order, nonhomogeneous differential equation.

$$
\frac{T - T_{\infty}}{T_i - T_{\infty}} = \exp(-at) + \frac{b/a}{T_i - T_{\infty}} [1 - \exp(-at)]
$$

If  $b = 0$ , this equation can be reduced to:

$$
\frac{T - T_{\infty}}{T_i - T_{\infty}} = \exp(-at)
$$

*3. General Lumped Capacitance Analysis*

*C. Convection Only with Variable Convection Coefficient:*

- $\triangleright$  In some cases, such as those involving free convection or boiling, the convection coefficient *h* varies with the temperature difference between the object and the fluid.
- The convection coefficient can often be approximated as follow:

$$
h = C(T - T_{\infty})^n
$$

where n is a constant and the parameter C has units of  $W/m^2$ .  $K^{(1+n)}$ 

$$
-C(T - T_{\infty})^n A_{s,c}(T - T_{\infty}) = -CA_{s,c}(T - T_{\infty})^{1+n} = \rho V c \frac{dT}{dt}
$$

$$
\frac{\theta}{\theta_i} = \left[ \frac{n C A_{s,c} \theta_i^n}{\rho V c} t + 1 \right]^{-1/n}
$$

#### *3. General Lumped Capacitance Analysis*

#### *Exampel-3*

Consider the thermocouple and convection conditions in Example-1, but now allow for radiation exchange with the walls of a duct that encloses the gas stream. If the duct walls are at 400 °C and the emissivity of the thermocouple bead is 0.9, calculate the steadystate temperature of the junction. Also, determine the time for the junction temperature to increase from an initial condition of 25  $\degree$ C to a temperature that is within 1  $\degree$ C of its steady-state value.



#### *3. General Lumped Capacitance Analysis*

#### *Exampel-3*

For steady-state conditions, the energy balance on the thermocouple junction has the form



### *3. General Lumped Capacitance Analysis*

#### *Exampel-3*

The temperature-time history, *T*(*t*), for the junction, initially at  $T_{(0)} = T_i = 25$  °C, follows from the energy balance for transient conditions:

$$
E_{\rm in} = \dot{E}_{\rm st}
$$
\n
$$
= [\hbar(T - T_{\infty}) + \varepsilon \sigma (T^4 - T_{\rm sur}^4)] A_s = \rho V c \frac{dT}{dt}
$$
\n
$$
= 400 \text{ W/m}^2 \cdot \text{K}
$$
\n
$$
T_{\rm sc} = 200 \text{°C}
$$
\n
$$
T_{\rm sc} = 200 \text{°C}
$$
\n
$$
T_{\rm sc} = 200 \text{°C}
$$
\n
$$
T_{\rm sc} = 2500 \text{ kg/m}^3
$$
\n
$$
C = 400 \text{ J/kg} \cdot \text{K}
$$
\n
$$
\varepsilon = 0.9
$$

The solution to this first-order differential equation can be obtained by numerical integration as follow:

 $T(4.9 \text{ s}) = 217.7 \text{°C}.$